

3.7.9

The energy equation yields, $h_1 - h_2 = h_f = 26 \text{ m}$

The Hazen-Williams eq'n can be written as: $h_f = KQ^m$

a) **One 30-cm pipe:** $K = (10.67L)/(D^{4.87} \cdot C^{1.85})$; $m = 1.85$

$$K = (10.67 \cdot 2000)/(0.30^{4.87} \cdot 140^{1.85}) = 804$$

$$h_f = 26 = KQ^m = (804)(Q)^{1.85}; \quad Q_{30} = 0.156 \text{ m}^3/\text{sec}$$

b) **Two 20-cm pipes:** $K = (10.67L)/(D^{4.87} \cdot C^{1.85})$; $m = 1.85$

$$K = (10.67 \cdot 2000)/(0.20^{4.87} \cdot 140^{1.85}) = 5790$$

$$h_f = 26 = KQ^m = (5790)(Q)^{1.85}; \quad Q_{20} = 0.0538 \text{ m}^3/\text{sec}$$

$$Q_{20s} = 2(Q) = 0.108 \text{ m}^3/\text{sec}; \quad \text{Not as much flow!!}$$

3.11.1

Contraction: $h_c = K_c[(V_2)^2/2g]$; V_2 is small pipe V

$$V_2 = Q/A = (0.106 \text{ m}^3/\text{s})/[\pi(0.075\text{m})^2] = 6.00 \text{ m/sec}$$

$$h_c = (0.15)[(6.00 \text{ m/s})^2/2 \cdot 9.81 \text{ m/s}^2] = 0.275 \text{ m}$$

Expansion: $h_E = [(V_1 - V_2)^2/2g]$; V_2 is now large pipe

$$V_2 = Q/A = (0.106 \text{ m}^3/\text{s})/[\pi(0.10 \text{ m})^2] = 3.37 \text{ m/sec}$$

$$h_E = [(6.00 \text{ m/s} - 3.37 \text{ m/s})^2/2 \cdot 9.81 \text{ m/s}^2] = 0.353 \text{ m}$$

Sudden expansion loss is much greater (by 28%).

3.11.3

The headloss is expressed as: $h_L = [K_v] (V)^2/2g$

$$\Delta P/\gamma = (14.5 \text{ lb/in}^2)(144 \text{ in}^2/\text{ft}^2)/62.3 \text{ lb/ft}^3 = 33.5 \text{ ft} = h_L$$

$$V = Q/A = (1.4 \text{ ft}^3/\text{s})/[\pi((1.5/12) \text{ ft})^2] = 28.5 \text{ ft/sec}; \text{ thus}$$

$$33.5 \text{ ft} = [K_v] (28.5 \text{ ft/s})^2/(2 \cdot 32.2 \text{ ft/s}^2)$$

$$K_v = 2.66$$

3.11.10

Applying the energy equation from the surface of the storage tank (1) to the outlet of the pipe (2) yields;

$$\frac{V_1^2}{2g} + \frac{P_1}{\gamma} + h_1 = \frac{V_2^2}{2g} + \frac{P_2}{\gamma} + h_2 + h_L; \text{ where } P_1 = P_2 = 0;$$

$h_L = [\sum K](V^2/2g)$; $h_f = 0$ (short pipe), $V_1 = h_2 = 0$. Thus

$$h_1 = [1 + \sum K](V^2/2g); \text{ where } V_2 = V \text{ (pipe } V);$$

$K_e = 0.5$; & $K_v = 10.0$. Rearranging the energy eq'n

$$V = [2g(h_1)/(1 + \sum K)]^{1/2} = [2 \cdot 32.2(h_1)/11.5]^{1/2} = 2.37h^{1/2}$$

For tank flow, $Q = d(\text{Vol})/dt = (\pi D^2/4)dh/dt$;

and pipe flow $Q = AV = (\pi d^2/4) [2.37h^{1/2}]$ where
 d = pipe diameter; D = tank diameter. Equating yields:

$$(\pi D^2/4)dh/dt = (\pi d^2/4)[2.37h^{1/2}]$$

$dt = [(D^2/d^2)dh] / [2.37h^{1/2}]$; integrating yields

$$t = (1/2.37)(D^2/d^2) \int_{h_1=5}^{h_2=10} h^{-1/2} dh$$

$$t = (1/2.37)[(16)^2/(0.667)^2] \cdot 2[(10)^{1/2} - (5)^{1/2}] = 450 \text{ sec}$$